## AMENDMENTS TO THE CLAIMS

- 1. (Currently Amended) A process for the manufacture of paraffinic hydrocarbons containing gasoline blending component, comprising hydrogenating in two steps characterized in that a mainly olefinic liquid feed-stock comprising olefins, and sulphur compounds as impurities, is hydrogenated in two steps in the presence of hydrogen and a noble metal catalyst on aluminium oxide support, and wherein in the first step the major part of olefins are converted and in the secondary step the remaining olefins and sulphur compounds react, and wherein a trickle-bed reactor is used in the first step and in the second step.
- 2. (Currently Amended) A process for the manufacture of paraffinic hydrocarbons containing gasoline blending component according to Claim 1, characterized in that wherein the hydrogen feed /olefin feed molar ratio is 0.9-2.0 0.9 ... 2.0, preferably 1.0 ... 1.5.
- 3. (Currently Amended) A process for the manufacture of paraffinic hydrocarbons containing gasoline blending component according to Claim 1 or 2, characterized in that wherein the feedstock contains comprises 80-97 wt % of  $C_8$  olefins, 3-20 wt % of  $C_{12}$  olefins, 0.1-7 wt % of  $C_9$ ,  $C_{10}$ ,  $C_{11}$  and heavier >  $C_{12}$  olefins and

optionally minor amounts of lighter  $C_6$ - $C_7$  olefins and 1-1000 wt-ppm of sulphur compounds, calculated as sulphur.

- 4. (Currently Amended) A process for the manufacture of paraffinic hydrocarbons containing gasoline blending component according to Claim 1, characterized in that wherein the feed-stock originates from a mixture obtained from a dimerization of butenes.
- 5. (Currently Amended) A process for the manufacture of paraffinic hydrocarbons containing gasoline blending component according to Claim 1, characterized in that wherein the feed-stock contains as sulphur compounds mainly sulphides, disulphides, thiophene tiophene and/or alkylthiophenes alkyltiophenes.
- 6. (Currently Amended) A process for the manufacture of paraffinic hydrocarbons containing gasoline blending component according to Claim 1, characterized in that wherein the noble metal catalysts comprises < 1 wt% of platinum or/and palladium.
- 7. (Currently Amended) A process for the manufacture of paraffinic hydrocarbons containing gasoline blending component according to Claim 1, characterized in that wherein the noble metal catalysts comprises < 1 wt% of platinum.

- 8. (Currently Amended) A process for the manufacture of paraffinic hydrocarbons containing gasoline blending component according to Claim 1, characterized—in that wherein the reaction temperature in the first step is in the range of 150-230°C and the pressure is in the range of 20-70 bar and in the second step the temperature is in the range of 180-300°C and the pressure is in the range of 20-70 bar.
- 9. (Currently Amended) A process for the manufacture of paraffinic hydrocarbons containing gasoline blending component according to Claim 1 characterized in that wherein the reaction heat is removed from the process and the reaction heat is used for preheating of incoming feed-stock to the a dimerization unit of butenes, or as an energy source for distillation columns of bottom boilers of dimerization unit of butenes.

## 10. (Cancelled)

11. (Currently Amended) A process for the manufacture of paraffinic hydrocarbons containing gasoline blending component according to Claim 1, characterized in that wherein in the first step the product stream is circulated in the reactor(s).

12. (New) A process for the manufacture of paraffinic hydrocarbons containing gasoline blending component according to Claim 1, wherein the hydrogen feed /olefin feed molar ratio is 1.0-1.5.